

Corrosion current determination with mass transfer limitation

I – INTRODUCTION

Several methods are available in EC-Lab[®] to measure the corrosion current:

- Stern Method (Tafel Fit),
- Stern and Geary method,
- VASP (VASP Fit),
- CASP (CASP Fit).

The first two methods are described in the Application Note #10 [1], the latter two in the Application Notes #36 [2] and #37 [3]. These methods are used in the case of general corrosion when the steady-state current potential curve satisfies the Stern (or Wagner-Traud) relationship:

$$I = I_{corr} \left(\exp\left(\frac{E - E_{corr}}{\frac{\beta_a}{\ln 10}}\right) - \exp\left(-\frac{E - E_{corr}}{\frac{\beta_c}{\ln 10}}\right) \right)$$
(1)

In this note, it is shown that the four different methods for determining corrosion parameters can be used in the case of general metal corrosion , limited by the mass transport of the oxidant. A new dummy cell that mimics such a system is used for this purpose.

II – CORROSION WITH MASS TRANS-FER LIMITATION

II - 1 I vs. E RELATIONSHIP

The corrosion rate is limited by mass transfer for instance in the presence of dissolved oxygen or when the cathodic reaction occurs very quickly[4]. The *I vs. E* relationship in these conditions is obtained with β_c tending to infinity in Eq. (1):

$$\beta_c \to \infty \Longrightarrow I = I_{corr} \left(\exp \left(\frac{E - E_{corr}}{\frac{\beta_a}{\ln 10}} \right) - 1 \right)$$
 (2)

The corresponding curve is given in Fig. 1.



Figure 1: Steady-state curves *I vs. E* and log *I vs. E* for the corrosion of a metal with mass transfer limitation of the oxydant.

II - 2 DUMMY CELL

a. Mészáros dummy cell

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It is convenient to use a dummy cell as model of known current *vs.* potential characteristics to check the different methods used to measure the corrosion parameters. Meszáros *et al.* have proposed a dummy cell for a corroding electrode, for which the cathodic partial process is diffusion-controlled [5]. The electrical circuit of this dummy cell is shown in Fig. 2.

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Figure 2: Mézáros' dummy cell [5].

As shown in Fig. 3 the cathodic plateau is not strictly horizontal. A Tafel Fit analysis yields to $\beta_c \approx 2 \times 10^4 \text{ mV}$ (Fig. 4) (¹).



Figure 3: Steady-state log | *I* | *vs. E* curve for the Mészáros dummy cell.

1e-20	relative error	Default	
Results	iterations		
Ecorr :	361,548	mV	
Icorr :	8,409	uΑ	
Πβ	113,8	mV	
Πβ.:	19523,4	mV	
χ^2		****	
χ/\sqrt{N}			
y^{2}/T^{2}			
Equivalent	Strategrades and Strategrades		
weight :	0,000	g/eq.	
Density :	0,000	g/cm3	
Surface are	ea : 0,001	cm ²	
Corrosion			
ate :	mi	mpy 🗸	

Figure 4: Tafel Fit Analysis of the Mészaros dummy cell. $B_c\approx 2.0{\times}10^4~mV.$

b. New dummy cell

A new, slightly more complicated, dummy cell (named BP dummy cell), is shown in Fig. 5. Its *I vs. E* curve shows a cathodic plateau which is strictly horizontal (Fig. 6).





Figure 6: Steady-state log | *I* | *vs. E* curve fot the BP dummy cell.

1e-20 1000	relative error iterations	Default	
Results			
Ecorr :	-781,062	mV	
Icorr :	74,731	uА	
β _a : β _a :	119,2	mV	
Øβc:	23522726	379 mV	
χ ²		xxxx	
χ/\sqrt{N}		XXXX	
χ^2/I^2		XXXX	
Equivalent weight :	0,000	g/eq.	
Density :	0.000	a/cm3	
Surface an	ea 0.001	cm ²	
Corrosion			

Figure 7: Tafel Fit Analysis of the BP dummy cell. I_{corr} = 74.731 µA, β_a = 119.2 mV, $\beta_c \approx 2.4 \times 10^{10}$ mV.

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Bio-Logic Science Instruments, 4 Rue de Vaucanson, 38170 Seyssinet-Pariset, FRANCE Tel: +33 476 98 68 31 – Fax: +33 476 98 69 09 <u>www.bio-logic.net</u> The different methods for determining the corrosion parameters are tested on the BP dummy cell.

III – STERN METHOD (TAFEL FIT)

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From the graphs displaying log |I| vs. E_{WE} , it is possible to determine the values of I_{corr} , E_{corr} , β_a and β_c by a simple graphical analysis. The Tafel fit, which is a Graph Analysis tool from EC-Lab[®] can automatically determine these values (Figs. 6 and 7). The value of I_{corr} , E_{corr} , β_a and β_c parameters are given in the caption of Fig. 7.

IV – STERN AND GEARY METHOD

The expression of the polarization resistance R_p can be defined as

$$R_p = \frac{1}{\frac{\mathrm{d}I}{\mathrm{d}E}} \tag{3}$$

Using for I the expression of Eq. (1) it gives

$$I_{corr} = \frac{\beta_a \beta_c}{R_{p,E_{corr}} \left(\beta_a + \beta_c\right) \ln 10}$$
(4)

And for a mass transfer limitation of the oxidant:

$$\beta_c \to \infty \Longrightarrow I_{corr} = \frac{\beta_a}{R_{p,E_{corr}} \ln 10}$$
 (5)

The value of R_p can be measured by the micropolarisation method (AN #10 [1]), or, better still, by plotting the impedance diagram of the dummy cell at rest potential (Fig. 8).



Figure 8: Nyquist diagram of the impedance of the BP dummy cell measured at the rest potential (x), δE =10 mV, $f \in [500 \text{ kHz}, 200 \text{ mHz}]$, and theoretical diagram of a R1/C1 circuit (line) with *R*1=624.4 Ω , *C*1=0.455.10⁻⁶ F.

The Nyquist diagram shown in Fig. 8 can be fitted using Z Fit [6]. The value of I_{corr} can be determined using the _a found previously by Tafel Fit analysis. With $R_p = R1 = 624.4 \Omega$ and $\beta_a = 0.118$ V it is obtained, using Eq. (5), $I_{corr} = 82.1 \mu$ A.

V – VASP METHOD

The VASP method is described in the Application Note #36 [3]. The VASP technique consists of the determination of the change of the measured polarization resistance R_p with the potential amplitude variation δE . R_p is determined by Electrochemical Impedance Spectroscopy measurements at a fixed and low enough frequency. For a negligible ohmic drop, R_p can be expressed by the following relation

$$\frac{1}{R_p} = I_{corr} \sum_{k=0}^{\infty} \frac{b_a^{2k+1} + b_c^{2k+1}}{2^{2k} k! (k+1)!} \delta E^{2k}$$
(6)

with $b_a = \ln 10/\beta_a$ and $b_c = \ln 10/\beta_c$. In the case where the corrosion is limited by mass transfer, it gives $\beta_c \rightarrow \infty \Rightarrow b_c \rightarrow 0$

$$\Rightarrow \frac{1}{R_p} = I_{corr} \sum_{k=0}^{\infty} \frac{b_a^{2k+1}}{2^{2k} k! (k+1)!} \delta E^{2k}$$
(7)

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Figure 9 shows the evolution of R_p with the amplitude of the potential amplitude δE .





VASP Fit		×
Selectic Trace : From poi X: Y: To point X: Y: Total po	nt: 0 1,011e-3 627,8 0H : 29 0,151 V 256,3 0H ints: 30	n ampl ∨ mr
Fit		
$\frac{1}{R_p} = I_{cc}$ $\odot Use$ $\bigcirc Use$	$\sum_{k=0}^{\infty} \frac{b_{s}^{2k+1} + 1}{2^{2k}k!} (\beta_{a} \text{ and } \beta_{c}$ $b_{a} \text{ and } b_{c}$	$\frac{b_{c}^{\text{and}}}{(k+1)!} v_{s}^{2k}$
param.	sel. value	unit
lcorr	84,1	μA
ßa	120,6	mV
ßc	0,1e12	mV
χ^2 χ/\sqrt{N} Iteration	96,28 7 1,792 s 92	
Calculate Minimize	Copy Sav Stop	/e Close

It is clear that R_p decreases with the amplitude, showing the non-linear behavior of the system. It is also clear that at the lowest amplitudes R_p tends to be constant. Fig. 10 shows the results obtained after the parametric fitting of the curve shown in Fig. 9. Note that the βc box is unchecked. The βc value is set to 10^{11} mV, as determined by Tafel Fit. The corrosion current is now 84.1 μ A.

VI – CASP METHOD

CASP is a new method for the determination of corrosion parameters [4]. The CASP method analyzes the non-linear response of an electrochemical system subjected to a sinusoidal potential of constant amplitude and frequency:

$$\Delta E(t) = E(t) - E_{corr} = \delta E \sin(2\pi f t)$$
(8)

The amplitude spectrum of the current *versus* time trace is shown in Fig. 11 for $\delta E = 50$ mV and f = 1 Hz.



Figure 11: Amplitude spectrum of the current response for the BP dummy cell. $\delta E = 50 \text{ mV}, f = 1 \text{Hz}.$

The relationships given in [3] are valid only when $b_c \neq 0$. The values of I_{corr} , b_a and b_c given in the CASP Window (Fig. 12) are wrong because in reality, $b_c = 0$. In this case, several relationships between I_{corr} , b_a and harmonic amplitudes are given in [7], including those below:

$$I_{corr} = \frac{\delta I_1 \left(\delta I_1 + \sqrt{\delta I_1^2 - 8\delta I_2^2} \right) - 4\delta I_2^2}{8 \left| \delta I_2 \right|}$$
(9)

$$b_a = \frac{1}{\delta E} \frac{\delta I_1 - \sqrt{\delta I_1^2 - 8\delta I_2^2}}{\left|\delta I_2\right|} \tag{10}$$

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CASP Fit	×
Selection	-
Trace : I vs. time	
From point : 0	
X: 111,2 s	
Y: -0,102 4e-3 mA	
To point: 195	
X: 121,2 s	
Y: -0,016 64 mA	
Total points : 196	
Input potential	5
$E - E_{corr} = \mathcal{V}_{\partial} \sin(2\pi f_{s} t)$	
Auto detect	
va: 150,000 mv	
fs: 1,000 Hz	
Distants	
511 : 0 000 21 mA	
512 0.001 07 mA	
6120,021 27 mA	
0150,013e-5 IIM	
Icorr: 176,6 μA	
ba: 15,22 V-1	
bc : -6,246 V-1	
βa: 151,3 mV	
βc: -368,7 mV	
error ~ 5,791 %	
	-
Laiculate Copy Save Clos	e

Figure 12: CASP window. $\delta E = 50 \text{ mV}, f = 1 \text{ Hz}.$

Using Eqs. (9) and (10) and values of δI_1 , δI_2 and δI_3 given in Fig. 12, the following values are obtained: $I_{corr} = 68.7 \ \mu A$, $b_a = 22.2 \ V^{-1}$.

VII – CONCLUSION

The values of the corrosion parameters obtained with the BP dummy cell with various different methods are shown in Tab. I. The mean value and the standard deviation of all the parameters are also shown in Tab I. The small values of the standard deviations show that the methods are compatible with one another, in the case where corrosion is limited by mass transfer of oxidant.

This application note showed that it is possible to build a dummy cell equivalent to a system whose cathodic kinetics are limited by the mass transfer of the oxidant. This dummy cell was coined a BP dummy cell. It was also

shown using the BP dummy cell, that the methods available in EC-Lab® to determine the corrosion rates (Tafel Fit, Stern Geary, VASP, CASP) can be used to determine the corrosion rate of a system for which the limitation of the mass transfer of the oxidant occurs.

Table I: Summary of the parameter values.						
Method	I _{corr} /μA	β₀/mV	<i>b</i> a/V ⁻¹			
Tafel Fit	74.7	119.2	19.4			
Stern Geary	82.1	-	-			
VASP	84.1	120.6	19.1			
CASP		120.4	22.2			
Mean value	77.4	119.9	20.5			
Standard deviation	±7.1	±0.81	±1.4			

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REFERENCES

1) Application note #10 "Corrosion current measurement for an iron electrode in an acidic solution"

2) Application note #36 "VASP: an innovative and exclusive technique for corrosion monitoring"

3) Application note #37 "CASP: a new method determination for the of corrosion parameters"

4) I. Epelboin, M. Keddam and H. Takenouti, J. Appl. Electrochem., 2 (1972) 71.

5) L. Mészaros, G. Mészaros and B. Lengyel, J. Electrochem. Soc., 141 (1994) 2068.

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